

Heat Transfer, Chapter 3 : Steady Heat Conduction Oct. 31 / 17

Thermal sci..

- Objs:
- 1) Understand concept of thermal resistance, develop resistance network for practical heat cond. prob.
 - 2) Multilayer wall, cylinder, sphere
 - 3) Identify when insulation increases heat transfer
 - 4) Conduction Shape Factor

Steady heat conduction in plane wall:

$$\dot{Q} = -KA \frac{dt}{dx}$$

$$\dot{Q}_{\text{cond,wall}} = \frac{KA(T_1 - T_2)}{L} \quad (\text{Watt}) \quad \text{or} \quad \left[\frac{(T_1 - T_2)}{R_{\text{wall}}} \right]$$

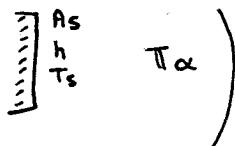
Thermal Resistance Concept :

$$I = \frac{V_1 - V_2}{R_e} \rightarrow \text{potential diff.}$$

Ohm's law

$$\dot{Q}_{\text{cond,wall}} = \frac{KA(T_1 - T_2)}{L}$$

Newton's Law of Cooling (convection):



$$\dot{Q}_{\text{conv}} = hA_s(T_s - T_\alpha)$$

$$= \frac{T_s - T_\alpha}{(1/hA_s)}$$

$$= \frac{T_s - T_\alpha}{R_{\text{conv.}}}$$

$$R_{\text{conv.}} = K/w \text{ or } ^\circ C/w$$

$$= \frac{(T_1 - T_2)}{(L/KA)}$$

$$= \frac{(T_1 - T_2)}{(R_{\text{wall}})}$$

where

$$R_{\text{wall}} = \frac{L}{KA}$$

$$\dot{Q}_{\text{rad}} = \epsilon\sigma A_s (T_s'' - T_{\text{surr}}'')$$

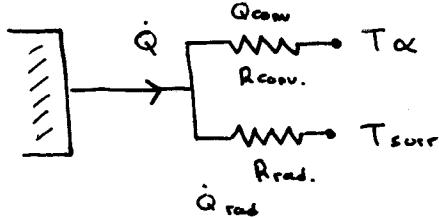
$$= \epsilon\sigma A_s [(T_s^2 - T_{\text{surr}}^2)(T_s^2 + T_{\text{surr}}^2)]$$

$$= \epsilon\sigma A_s [(T_s - T_{\text{surr}})(T_s + T_{\text{surr}})(T_s^2 + T_{\text{surr}}^2)]$$

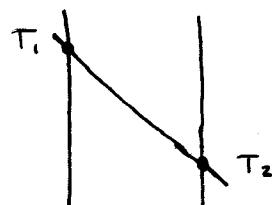
$$\left[\left(\frac{T_s - T_{\text{surr}}}{R_{\text{rad}}} \right) \right]$$

$$R_{\text{rad}} = \frac{1}{h_{\text{rad}} A_s}$$

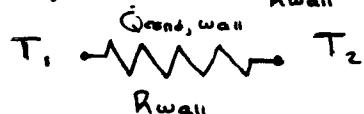
$$h_{\text{rad}} = \epsilon \sigma (T_2^2 + T_{\text{sur}}^2)(T_s + T_{\text{sur}}) \quad (\text{in } \text{W/m}^2 \cdot \text{K})$$



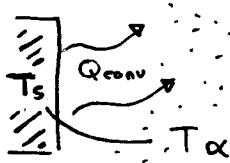
$$\dot{Q} = \dot{Q}_{\text{conv.}} + \dot{Q}_{\text{rad}}$$



$$\dot{Q}_{\text{cond, wall}} = \frac{T_1 - T_2}{R_{\text{wall}}}$$



Convection

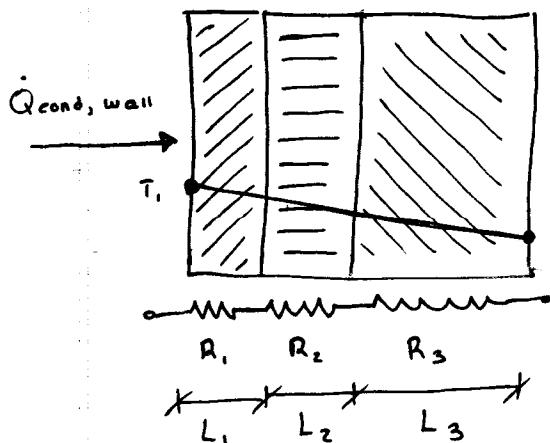


$$\dot{Q}_{\text{conv.}}$$

$$T_s \xrightarrow{\text{Q}_{\text{conv.}}} T_{\alpha}$$

$$R_{\text{conv.}} = \frac{1}{h A_s}$$

$$h_{\text{comb}} = h_{\text{conv.}} + h_{\text{rad}}$$

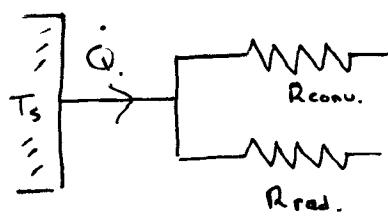


$$\dot{Q}_{\text{cond}} = \frac{T_1 - T_4}{R_{\text{TOTAL}}}$$

$$R_{\text{TOTAL}} = R_{\text{wall}_1} + R_{\text{wall}_2} + R_{\text{wall}_3}$$

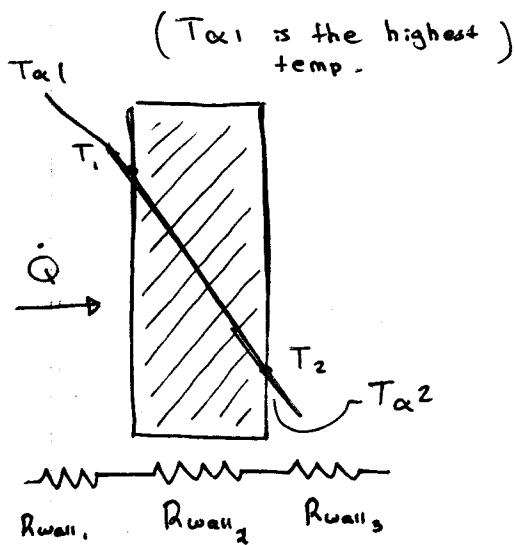
$$R_{\text{wall}_1} = \frac{L}{K_1 A} \quad ; \quad R_{\text{wall}_2} = \frac{L}{K_2 A}$$

$$R_{\text{wall}_3} = \frac{L}{K_3 A}$$



$$\frac{1}{R} = \frac{1}{R_1} + \frac{1}{R_2} + \dots + \frac{1}{R_n}$$

$$\frac{1}{R_{\text{TOTAL}}} = \frac{1}{R_{\text{conv}}} + \frac{1}{R_{\text{rad}}}$$



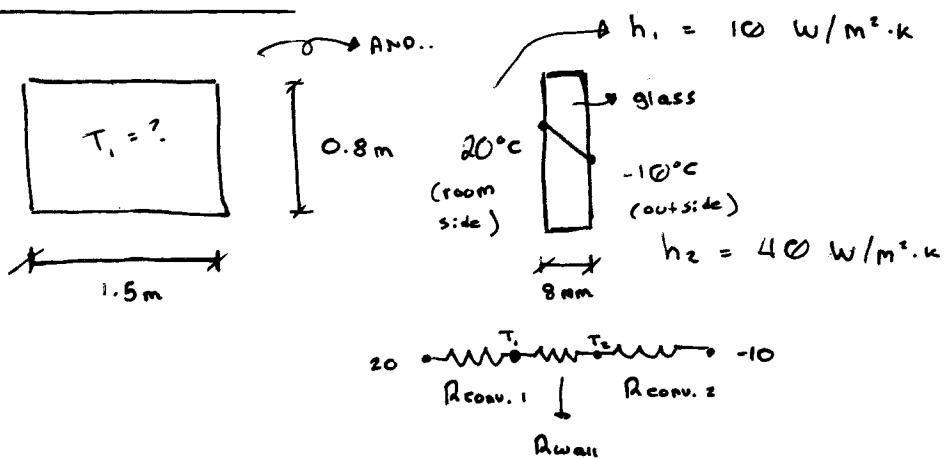
$$\dot{Q} = \frac{T_{\alpha 1} - T_{\alpha 2}}{R_{\text{TOTAL}}} \quad \begin{matrix} \frac{1}{hA} \\ \frac{1}{kA} \end{matrix}$$

$$R_{\text{TOTAL}} = R_{\text{conv1}} + R_{\text{wall}} + R_{\text{conv2}}$$

$$\dot{Q} = hA(T_{\alpha 1} - T_1) = \frac{kA(T_1 - T_2)}{L}$$

$$= hA(T_2 - T_{\alpha 2})$$

Example 3-2 :



$$\dot{Q} = \frac{T_{\alpha 1} - T_{\alpha 2}}{R_{\text{TOTAL}}}$$

$$R_{\text{conv}, 1} = \frac{1}{h_1 A} = \frac{1}{10 \times (0.8 \times 1.5)} = 0.08333 \text{ }^{\circ}\text{C/W}$$

$$R_{\text{wall}} = \frac{L}{kA} = \frac{(0.008)}{(0.78)(0.8 \times 1.5)} = 0.00855 \text{ }^{\circ}\text{C/W}$$

$$R_{\text{conv}, 2} = \frac{1}{h_2 A} = \frac{1}{40 \times (0.8 \times 1.5)} = 0.02083 \text{ }^{\circ}\text{C/W}$$

$$\dot{Q} = \frac{20 - (-10)}{(0.08333)}$$

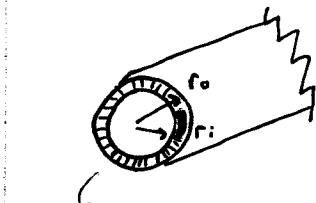
$$\boxed{\dot{Q} = 266 \text{ W}}$$

$$\dot{Q} = \frac{T_{\alpha 1} - T_1}{R_{\text{conv}, 1}}$$

$$\therefore \boxed{T_1 = -2.2 \text{ }^{\circ}\text{C}}$$

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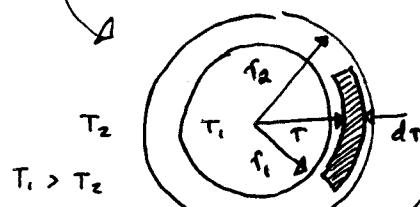
Thermal Sci.



Heat conduction in Cylinders:

$$\dot{Q}_{\text{cond}} = -KA \frac{dT}{dx}$$

$$(1D): \dot{Q}_{\text{cond, cyl}} = -KA \frac{dT}{dx}$$



$$\int_{r_i}^{r_o} \frac{\dot{Q}_{\text{cond, cyl}}}{A} dr = - \int_{T_1}^{T_2} K dT$$

$$A = 2\pi r L$$

$$\int_{r_i}^{r_o} \dot{Q}_{\text{cond, cyl}} \frac{dr}{r} = -2\pi K L \int_{T_1}^{T_2} dT$$

$$\Rightarrow \dot{Q}_{\text{cond, cyl}} \ln \frac{r_o}{r_i} = -2\pi K L T \Big|_{T_1}^{T_2}$$

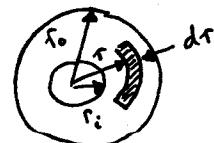
$$\dot{Q}_{\text{cond, cyl}} (\ln r_o - \ln r_i) = -2\pi K L (T_2 - T_1)$$

$$\dot{Q}_{\text{cond, cyl}} \left(\ln \left(\frac{r_o}{r_i} \right) \right) = 2\pi K L (T_1 - T_2)$$

$$\dot{Q}_{\text{cond, cyl}} = \frac{T_1 - T_2}{R_{\text{cyl}}} \quad \therefore R_{\text{cyl}} = \frac{\ln \left(\frac{r_o}{r_i} \right)}{2\pi K L}$$

$$\underline{\text{For sphere:}} \quad \dot{Q}_{\text{cond, sphere}} = -KA \frac{dT}{dr}$$

$$\dot{Q}_{\text{cond, sphere}} = \frac{T_1 - T_2}{R_{\text{sphere}}}$$



$$R_{\text{sphere}} = \frac{r_o - r_i}{4\pi r_i r_o K}$$

$$R_{\text{wall}} = \frac{L}{KA}$$

$$R_{\text{cylinder}} = \frac{\ln \left(\frac{r_o}{r_i} \right)}{2\pi K L}$$

$$R_{\text{sphere}} = \frac{r_o - r_i}{4\pi r_i r_o K}$$

Cartesian coordinate

Cylindrical

Spherical

Plane Wall

cylinder

Sphere

$$\dot{Q}_{\text{conduction}} = \frac{T_1 - T_2}{R_{\text{wall}}}$$

$$\dot{Q}_{\text{conduction, cyl}} = \frac{T_1 - T_2}{R_{\text{cyl}}}$$

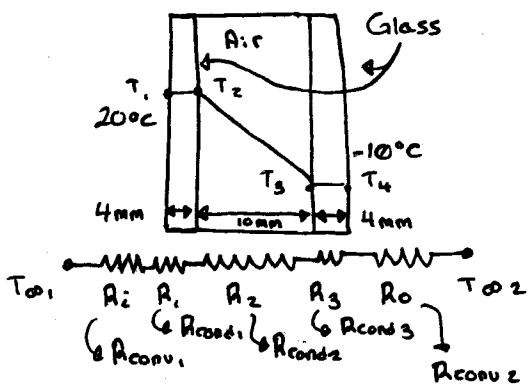
$$\dot{Q}_{\text{conduction, sphere}} = \frac{T_1 - T_2}{R_{\text{sphere}}}$$

Example 3.3 - (Textbook)

$$A = \emptyset.8 \text{ m} \times 1.5 \text{ m}$$

$$t = 4 \text{ mm} = \emptyset.004 \text{ m} \quad (\text{two panes}), \text{ with } \emptyset.01 \text{ m air gap.}$$

$$k = 0.78 \text{ W/m.K}$$



$$R_i = R_{\text{conv},1} = \frac{1}{hA} \Rightarrow \frac{1}{(0.08333)(0.8 \times 1.5)}$$

$$R_i = 0.08333 \text{ °C/W}$$

$$R_1 = R_{\text{cond},1} = \frac{L}{KA} = \frac{(0.004)}{(0.78)(0.8 \times 1.5)}$$

$$R_1 = 0.00427 \text{ °C/W} = R_3$$

$$R_2 = R_{\text{cond},2} = \frac{L}{KA} = \frac{(0.010)}{(0.78)(0.8 \times 1.5)}$$

$$R_2 = 0.3205 \text{ °C/W}$$

$$R_o = R_{\text{conv},2} = \frac{1}{hA} = \frac{1}{(0.02083)(0.8 \times 1.5)}$$

$$R_o = 0.02083 \text{ °C/W}$$

$$R_{\text{TOTAL}} = R_{\text{conv},1} + R_{\text{conv},2} + \dots$$

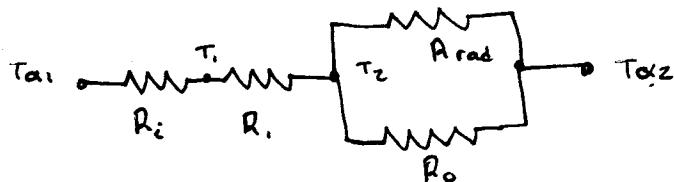
$$\dots + R_{\text{cond},1} + R_{\text{cond},2} + R_{\text{cond},3}$$

$$R_{\text{TOTAL}} = 0.4332 \text{ °C/W}$$

$$\dot{Q} = \frac{T_{\infty 1} + T_{\infty 2}}{R_{\text{TOTAL}}} \Rightarrow \frac{20 - (-10)}{0.4332} = 69.2 \text{ W}$$

$$\begin{aligned} \therefore T_i &= T_{\infty 1} - \dot{Q}R_{\text{conv},1} \\ &= 20 - 69.2 \times (0.08333) \\ \therefore T_i &= 14.2^\circ\text{C} \end{aligned}$$

Example 3.7 - (Textbook)



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Cont'd.

$$A_1 = \pi D_1^2 = \pi (3^2) = 28.3 \text{ m}^2$$

$$A_2 = \pi D_2^2 = \pi (3.04^2) = 29 \text{ m}^2$$

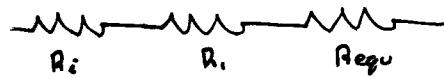
$$h_{rad} = \epsilon \sigma (T_s^{50^\circ\text{C}} + T_{surf}^{22^\circ\text{C}})$$

$$\therefore h_{rad} = 5.34 \text{ W/m}^2\cdot\text{K}$$

$$R_i = R_{conv-i} = \frac{1}{h_i A_i} = \frac{1}{80 \times 28.3} = 0.000442 \text{ } ^\circ\text{C/W}$$

$$R_i = R_{sph} = \frac{r_2 - r_1}{4 \pi k_i r_i K} = (\dots) = 0.000047 \text{ } ^\circ\text{C/W}$$

$$\frac{R_{rad}}{R_o} R_{equ.} \frac{1}{R_{equ.}} = \frac{1}{R_o} + \frac{1}{R_{rad}} \therefore R_{equ.} = 0.00225 \text{ } ^\circ\text{C/W}$$



$$\therefore R_{total} = 0.00274 \text{ } ^\circ\text{C/W}$$

$$\dot{Q} = \frac{T_{\alpha_2} - T_{\alpha_1}}{0.00274} = 8029 \text{ W}$$

$$\dot{Q} = \frac{T_{\alpha_2} - T_2}{R_{equ.}} \Rightarrow T_2 = 4^\circ\text{C}$$

$$\begin{aligned} \text{In 24 hours: } \dot{Q} &= \frac{\dot{Q}}{\Delta t} \Rightarrow Q = \dot{Q} \cdot \Delta t \\ &\Rightarrow (8029)(24)(60)(60) \\ &= 693700 \text{ kJ} \end{aligned}$$

Ice's latent heat of fusion = 333.7 kJ

$$\text{Mass of ice} \quad \therefore M_{ice} = \frac{Q}{h_{fus}} = \frac{693700 \text{ kJ}}{333.7 \text{ kJ/kg}} = 2079 \text{ kg}$$

Example 3-8

